

# Improving Yield and Throughput of Downstream Processing: Biomass Removal & Capture Steps



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Dusseldorf – Post Conference Workshop**

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– Copenhagen, Denmark**

# Effect of Reducing Number Operational Units



- Increased yield
- Simpler PD/ process (facility & operations)
- Reduced CapEx & OpEx
- Increased throughput of product / products (facility utilisation)
- Lower burden of QC/QA

# Current Manufacturing Trends



- 3 step chromatography to 2 step
- Disposable unit operations eliminate CIP
- Disposable chromatography eliminates repacking
- Process integration - Eliminate UF/DF buffer exchange & concentration step, hold tanks.
- On-line dilution replaces buffer prep.

# Current Manufacturing Trends



- 3 step chromatography to 2 step
- Disposable unit operations eliminating CIP
- Disposable repair
- Eliminating containers
- Process integration eliminates hold tanks
- On-line dilution replaces ss tanks

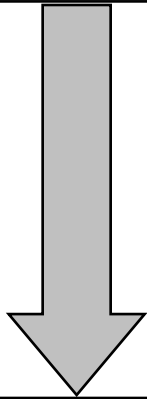
**FURTHER  
IMPROVEMENTS**

## *Intravenous immunoglobulin (IVIg) manufacturing*

- IVIG sold at \$50/g (hyperIVIg, \$200-300/g)
- Plant capacities range from 250 kg to 5 tonnes per annum.
- (Yield critical, high demand for product)
- Chromatography increasingly used.

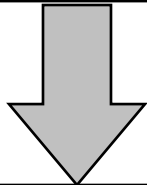
# COHN FRACTION II+III PROCESSING

Ethanol Precipitate  
II+III resolubilised



Depth Filtration

Sterile Filtration



Chromatography

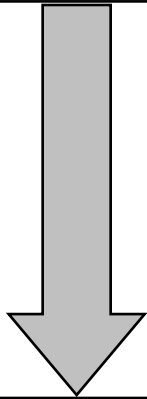


*Similarities to high titre  
mammalian cell culture*

- +10g/L IgG
- Large amount of sticky insolubles
- Clarification results in yield losses (5-10%)
- Batch processing time important

# COHN FRACTION II+III PROCESSING

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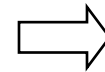
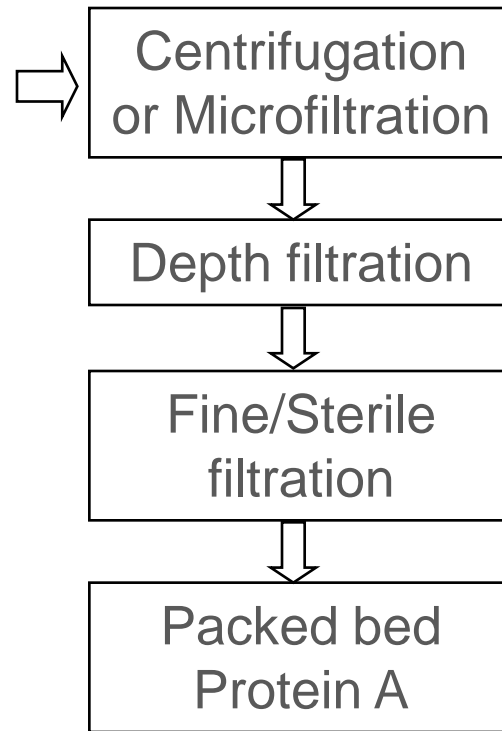


**IgG Direct  
CAPTURE**

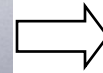


- Elimination of depth filtration/fine filtration
- 10% increase yield
- 1 extra batch per week possible

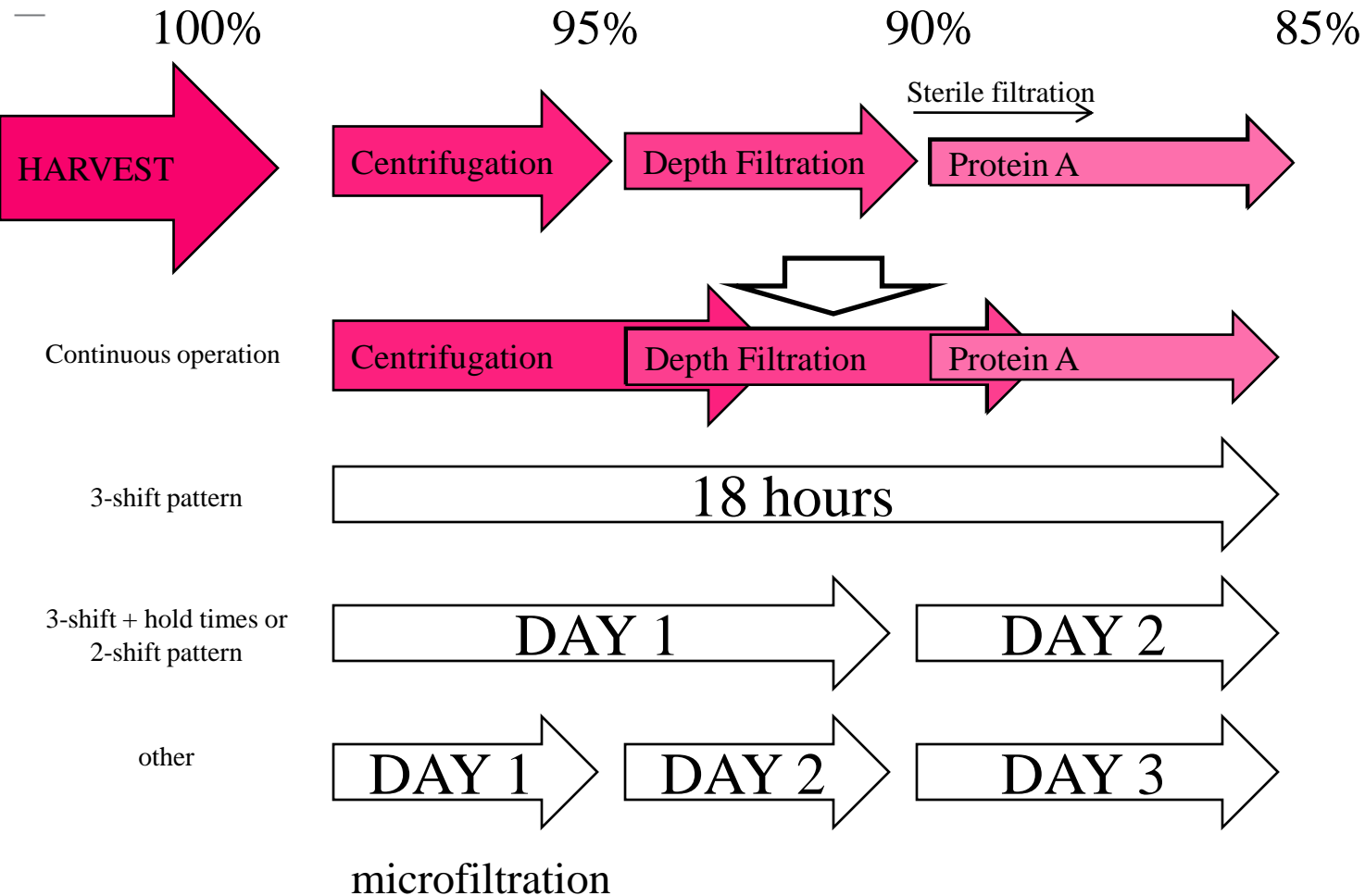
# Direct Capture For Monoclonals



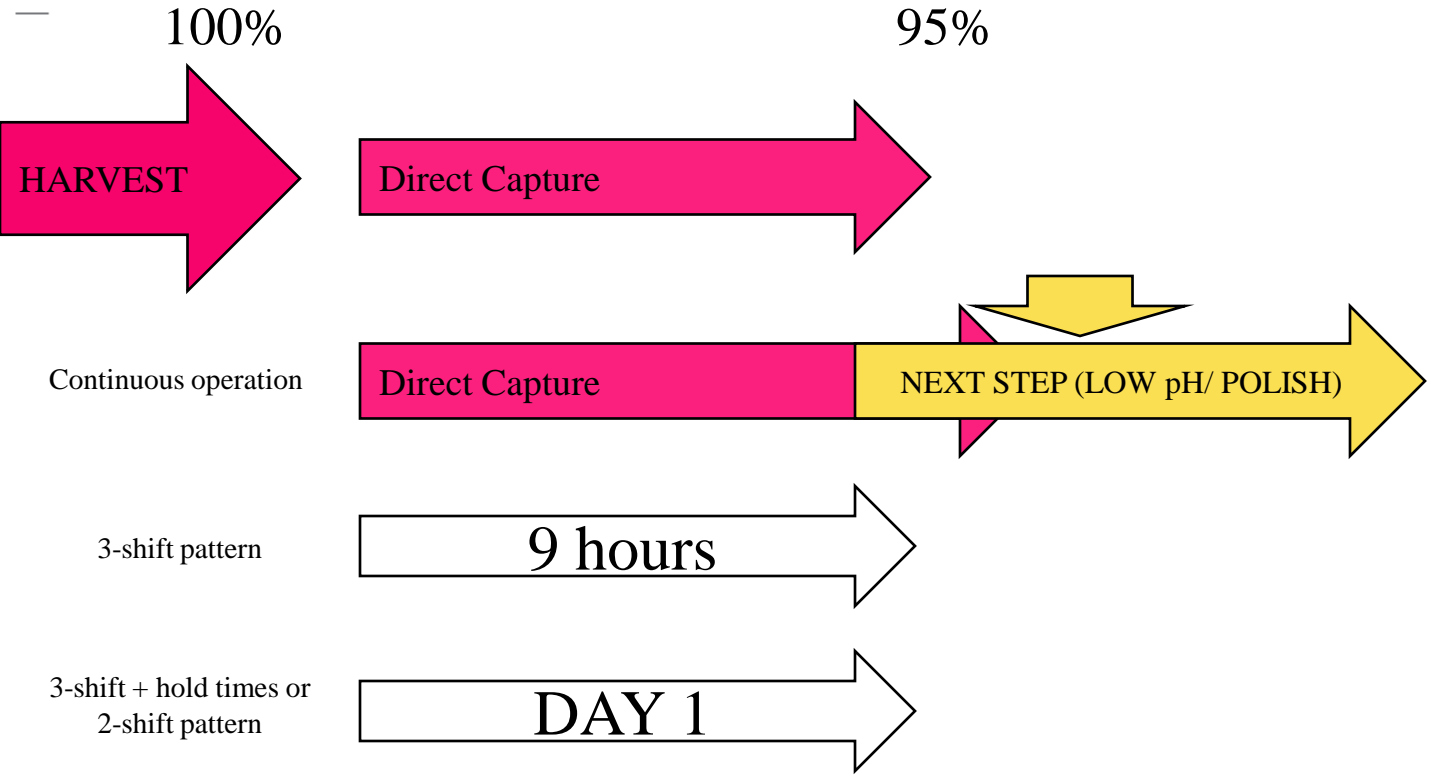
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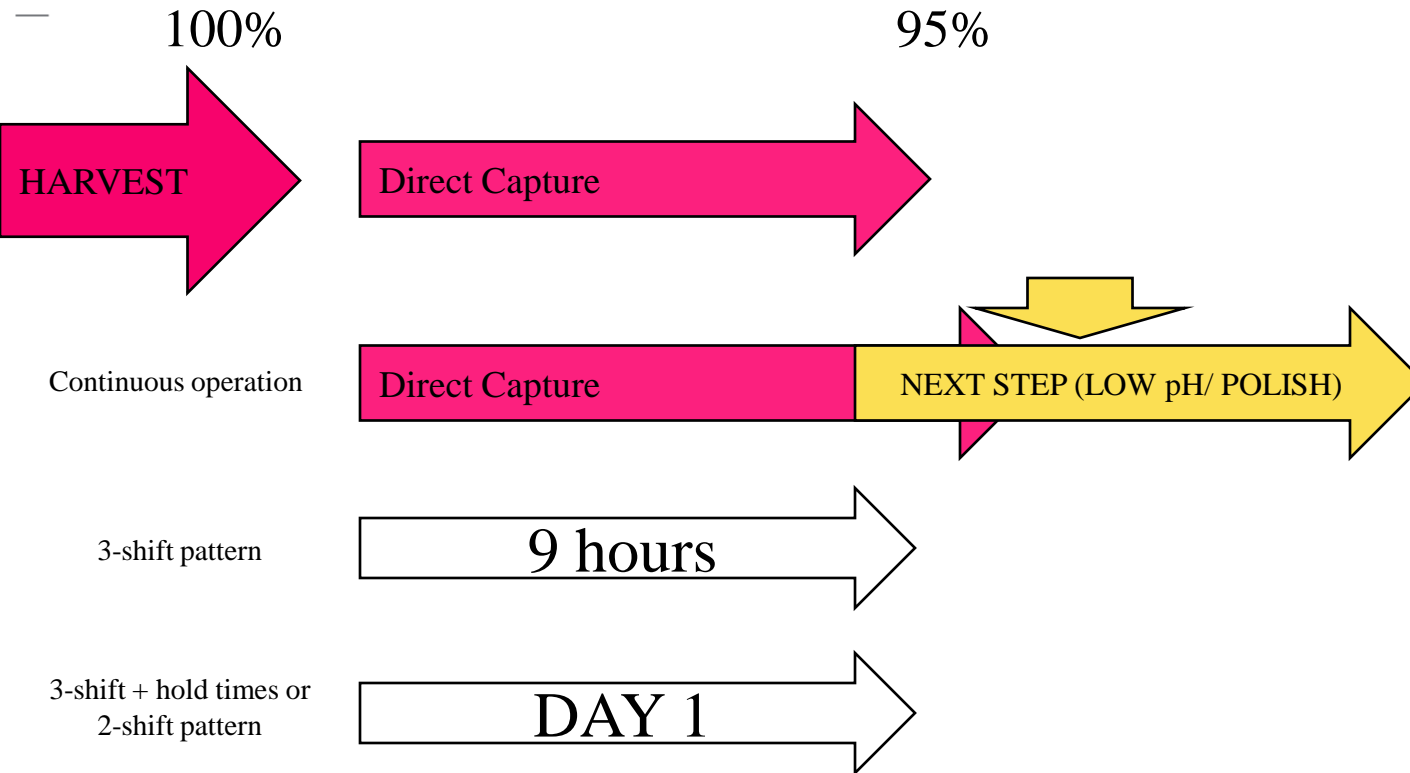
# Value of Throughput in Different Facilities



# Facility Utilisation with Direct Capture

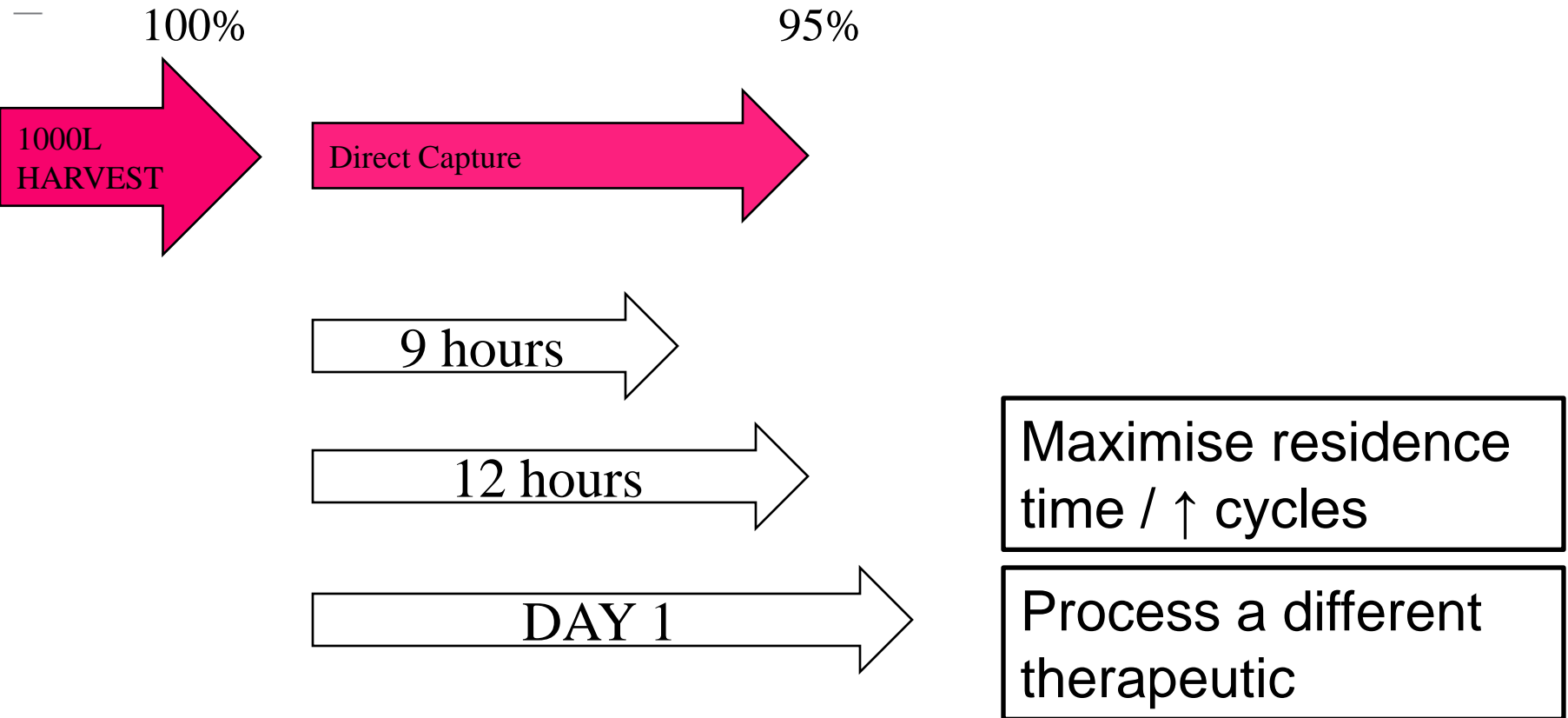


# Facility Utilisation with Direct Capture

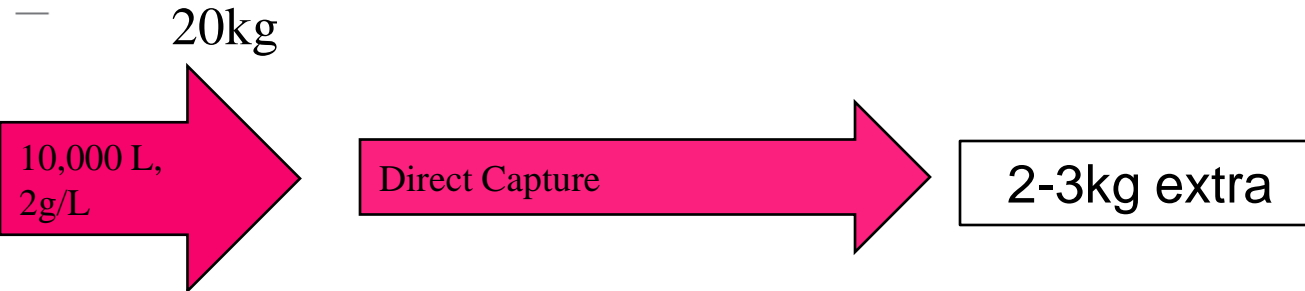


- Improve facility scheduling / extra bioreactor runs

# Effect of Single-Use Direct Capture on Facility Utilisation



# Yield Increase $10 \pm 5\%$



- Sales value (\$2000/g) = **\$2-3 million per bioreactor run**
- Manufacturing value (\$150/g) = **\$300,000-\$450,000 /bioreactor**
- Increase facility production capacity
- Number of products / projects ?
- Lower burden of QC samples ?
- etc


# Direct Capture Processing Advantages

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- Throughput (Productivity)
- Yield
- Footprint
- Cost of Goods

# Considerations Of Future Processes



High Titre Feedstocks  
Smaller reactors  
Multi-product facilities



## Clarification issues

- Process development required
- Increased solids entrapment (dead-end) vs processing time (TFF)
- Increased single use consumable cost (disposable centrifuge/depth filtration)



# Cost of Goods



	Contribution	Comments
No requirement for clarification	C of G ↓	Major effect = yield increase
	Cap Ex ↓	Eliminate centrifugation/depth filtration/fine filtration units (disposable clarification)
No CIP (adsorbent or operating system)	C of G ↓	WFI, acid, alkali, steam, time
	Cap Ex ↓	Validation, CIP equipment, tanks
Flexibility / Facility Utilisation		Optimal use of clean rooms

# Economic Considerations



	Contribution	Comments
Consumable cost (low number of cycles)	C of G ↑	Adsorbent cost usually mitigated by cycling
Waste management	C of G ↑	Incineration costs

# Economic Considerations



	Contribution	Comments
Consumable cost (low number of cycles)	C of G ↑	Adsorbent cost usually mitigated by cycling. <b>However, Direct Capture eliminates consumable costs of clarification steps.</b>
Waste management	C of G ↑	Incineration costs. <b>Direct Capture eliminates extra waste from clarification steps.</b>

# Direct Capture Technology

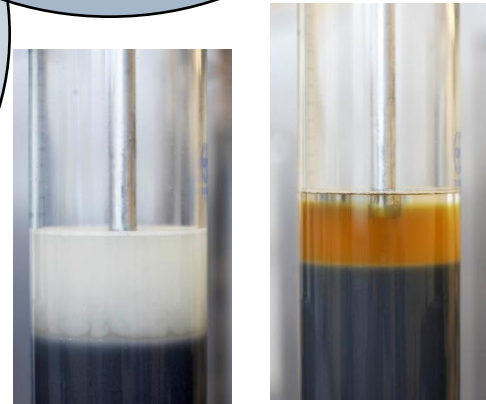
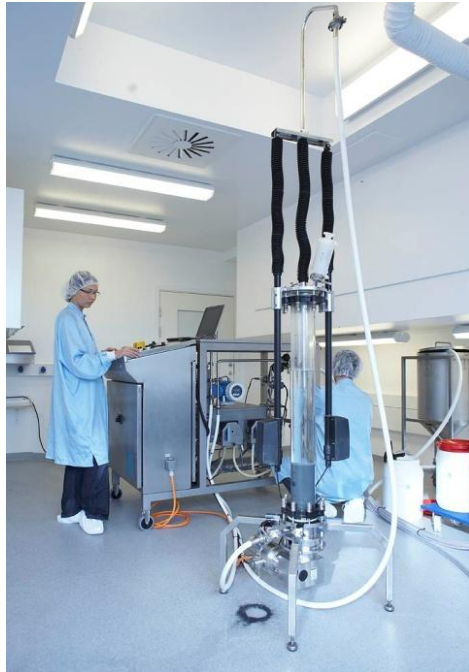
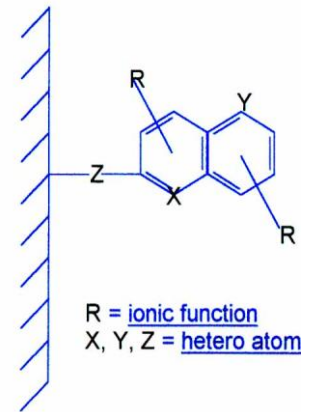


## CRITICAL INNOVATION AREAS

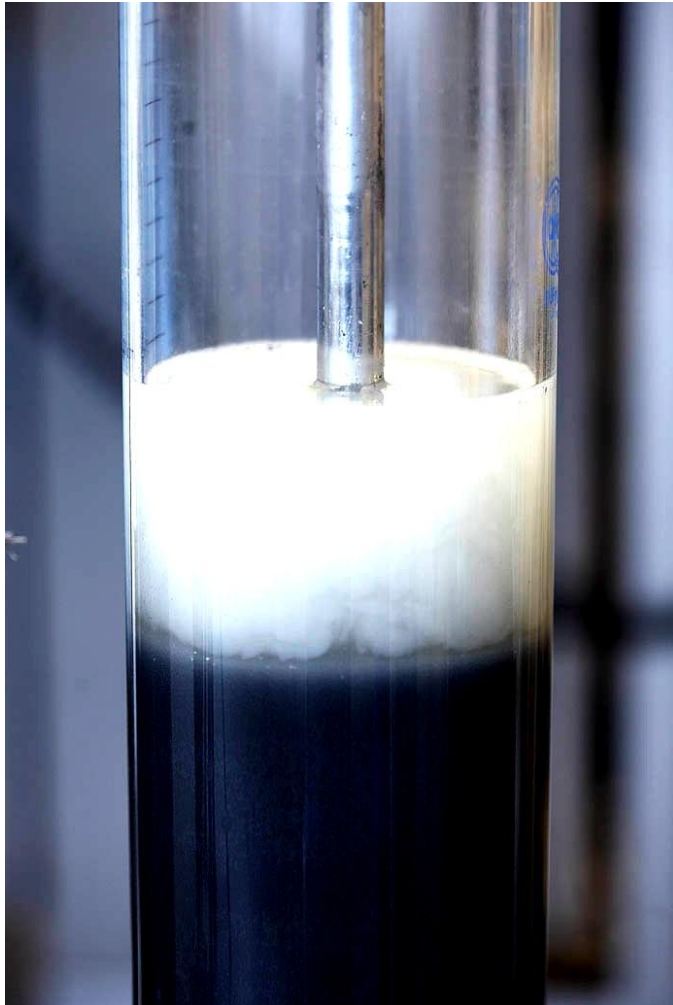
Engineering/  
Operating  
Systems

Ligand  
Biochemistry

Expanded  
Bed  
Adsorbents



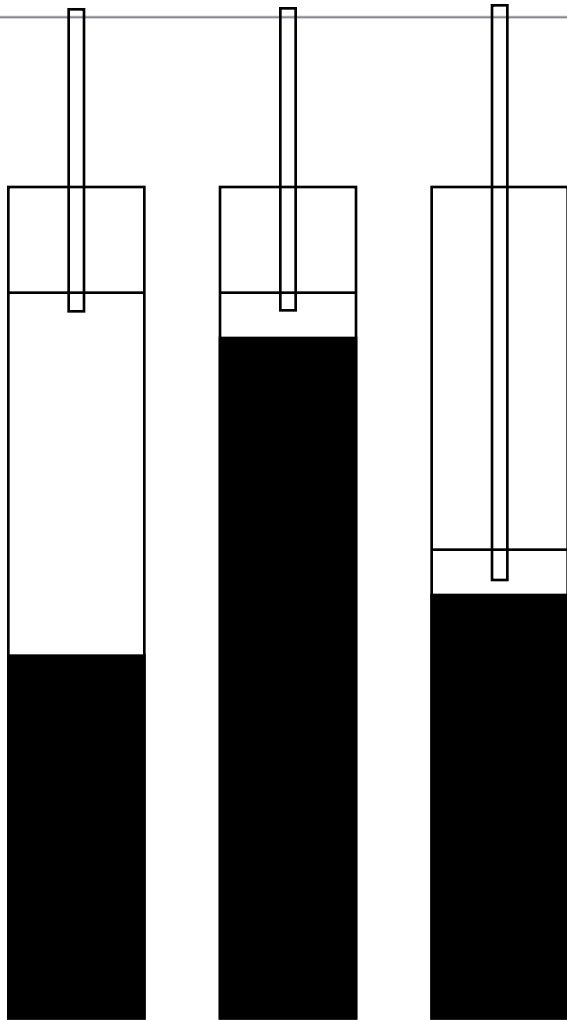
# Second Generation – EBA v 2.0



## Reduced buffer consumption

- Tall column (50cm sbh)
- Reduce expansion during washing and elution

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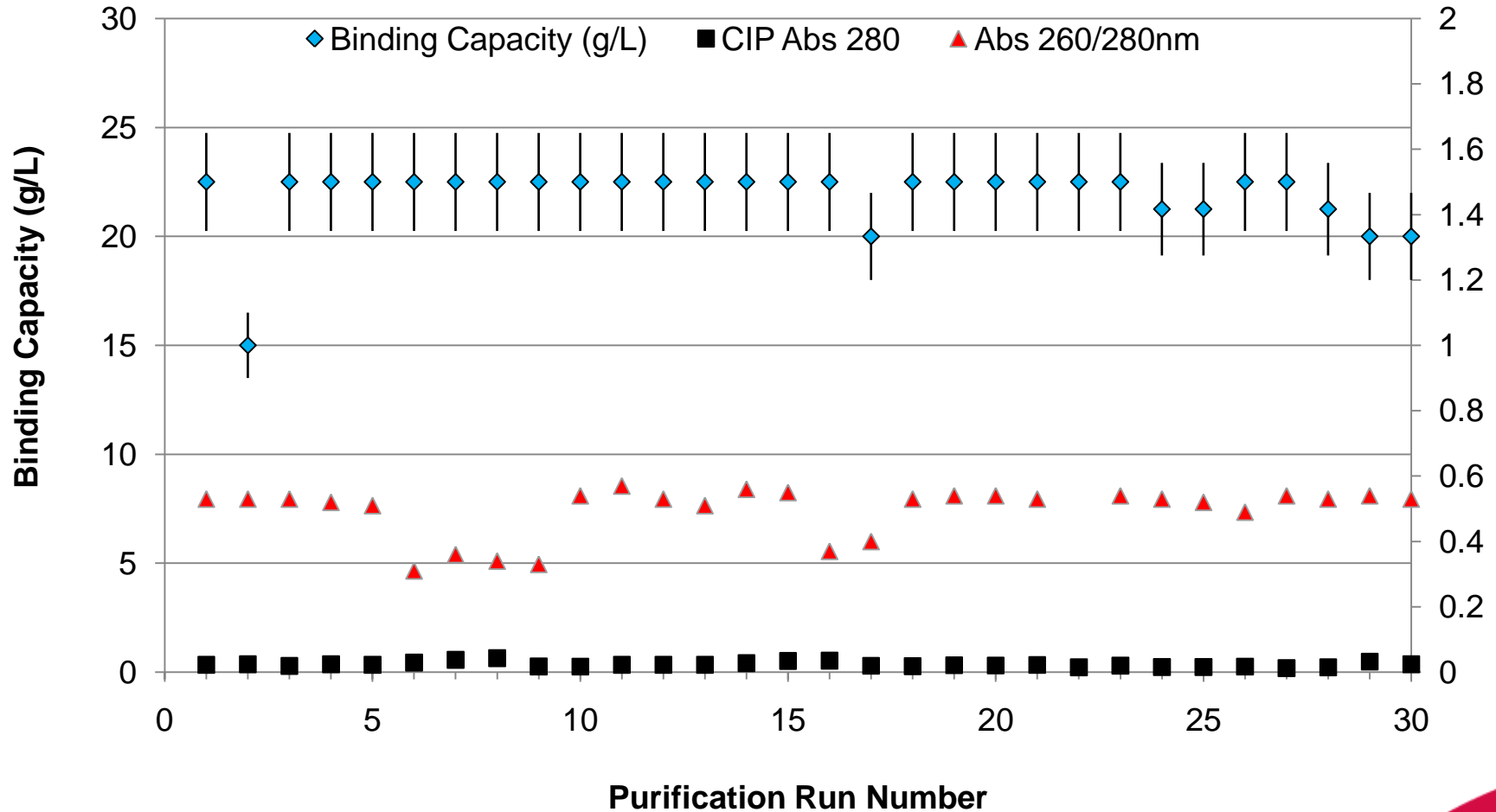


### Reduced buffer consumption

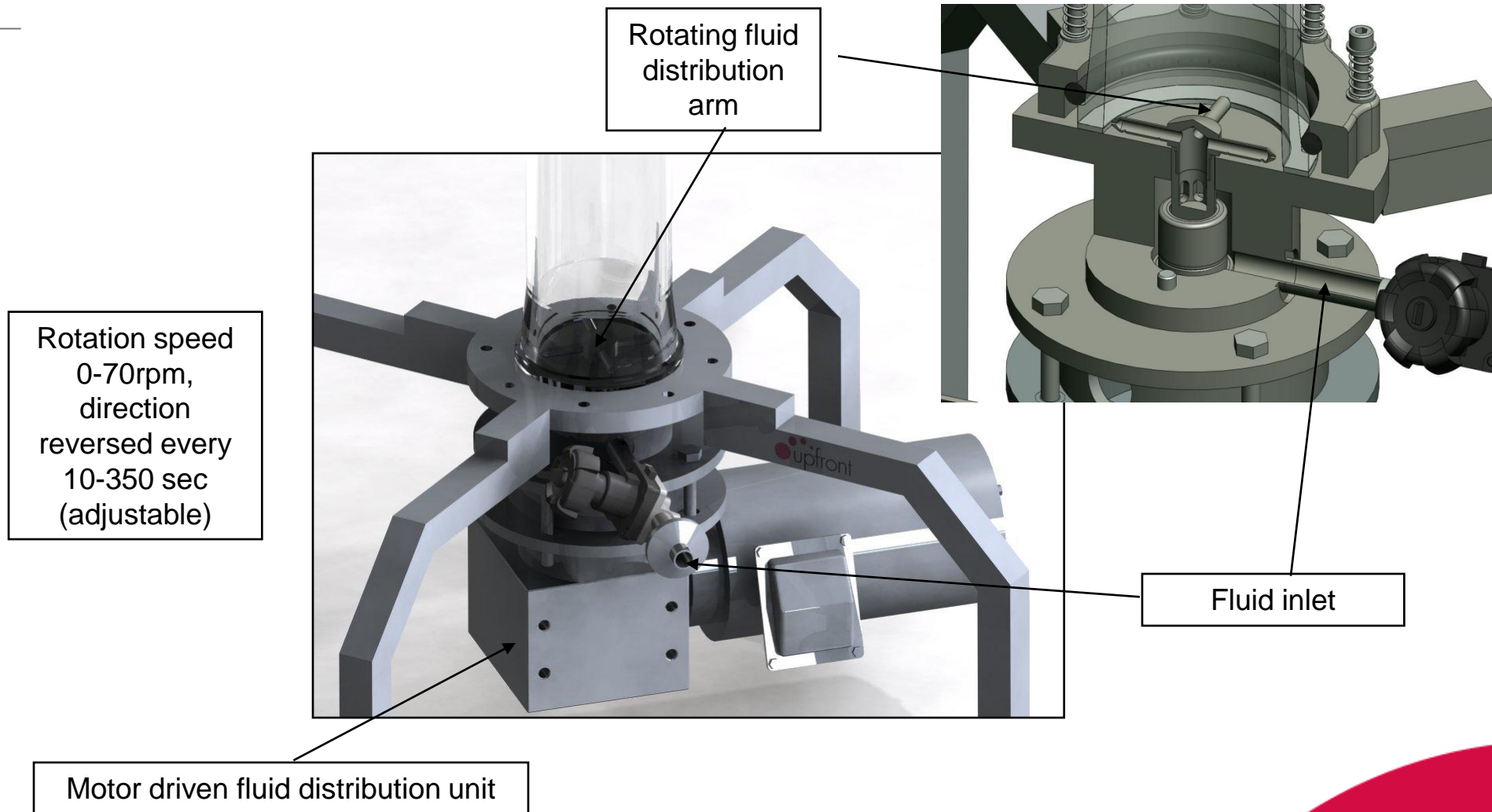
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- Reduce expansion during washing and elution

settled    load    elute

# Repeated Cycles Data – 5% w/v Yeast Homogenate, 1g/L IgG (50mM NaOH, 1M NaCl CIP)



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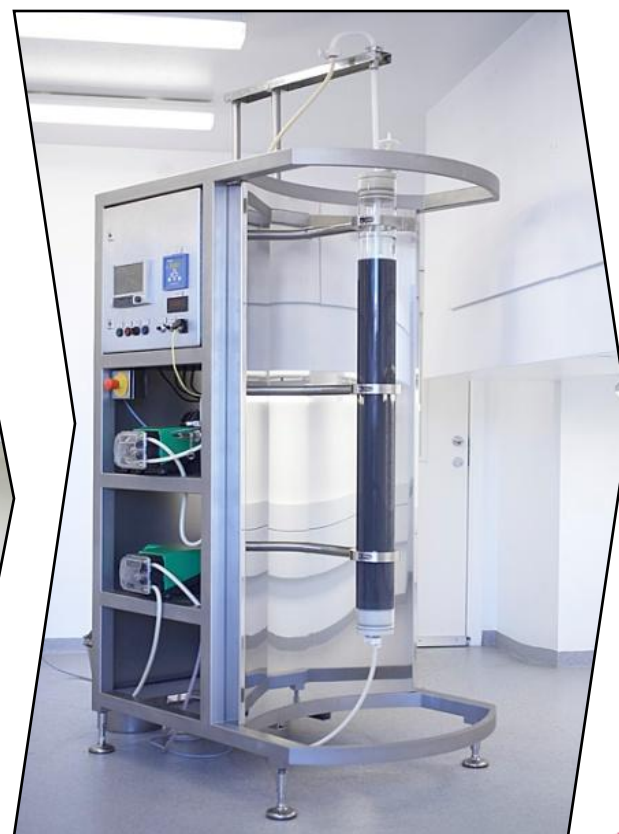
## One Campaign !!



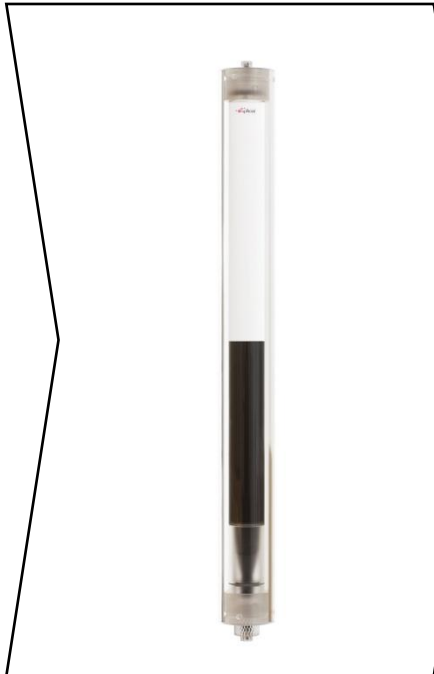
## Scale-Up, Robustness, Ease of Operation

- Industrial technology came first
- 1cm – 150cm scale up

# Process Development Tools



# Process Development Tools



# Rhobust Flex Operating System & Production Scale



# cGMP *Rhobust*<sup>TM</sup> EBA Features



FEATURE	PROCESS BENEFIT
Increased Density Beads	High flow rates Stable bed High inertia to changes
No porous plates	Processing crude or unstable feedstocks without clogging
Mixed mode affinity ligands	Increase selectivity, reduce non-specific binding
Inherent positioning of beads	No column packing/repacking

# cGMP Rhobust™ EBA Features



FEATURE	PROCESS BENEFIT
High temperature (60 °C) 1M NaOH <b>facilitated</b>	Thorough clean-in-place facilitated Long adsorbent lifetime
High Fluid Velocity Cleaning (spray balls, flow distribution jets)	No low flow areas, no dead spots Easy to remove adsorbent
Proprietary dual pump operation	Inside of column equilibrated with atmospheric pressure
Tall (1 m, 2 m, 3m), large columns (1,5 m diam. = 1,700 L-7,000 L)	Minimise wash & elution volumes Minimise number of cycles

- ✓ ISO 9001 certified since 2003
- ✓ Provide regulatory support file data
- ✓ Clean room manufacturing
- ✓ Present production capacity of 1000's litre per customer
- ✓ No animal raw materials
- ✓ FDA food approved since 1998

